## The advantages of the vacuum system operating with mixing (direct contact) condensers are:

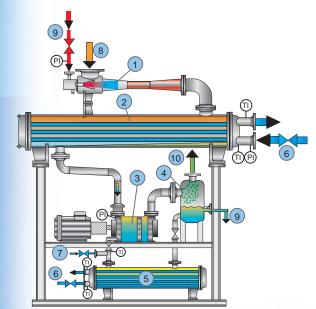
- very efficient due to direct contact between the process medium and the cooling medium
- low investment costs compared to indirect cooling
- simple and easy operation
- proven technology

## Hybrid vacuum systems as skid mounted unit

booster, a surface condenser and a popular for drying applications. The system is called hybrid system and is a

A vacuum system comprising a small customised solution. A non-barometric liquid ring vacuum pump as final stage of this design. A horizontal installation installed as skid mounted unit is very of the surface condenser increases the risk of pollution.





### **Design parameter**

- 100 kg/h water vapour + 5 kg/h air @ 50 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37 °C	Electrical energy (kW)
36	12	3.3

- 2 surface condenser
- 3 liquid ring vacuum pump (lrvp)
- 5 service water re-cooler (Irvp)
- 6 cooling water
- 7 fresh water (Irvn)

- 10 gas outlet separator (Irvp)

## The advantages of the vacuum system operating with surface condensers – compared to the conventional ones using mixing (direct contact) condensers – are:

- strict separation of cooling water and process medium
- environment-friendly e.g. low air pollution and clean cooling tower
- easy cleaning during operation
- proven technology supported by positive customer feedback

Körting vacuum systems for drying, neutralisation and bleaching of edible oil





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# Mixing (direct contact) condenser

That is why conventional vacuum systems operating with mixing condensation are still very popular for this application.



of this kind of vacuun



# Surface condenser

The initial idea for developing a vacuum system with indirect condensation was the requirement of environment-friendly systems in barometric and non-barometric design



Compared to conventional systems - with mixing (direct contact) condensers - the somewhat higher investment costs for such systems are quickly paid back due to increased environmental protection.

Positive feedback from customers and an increased number of inquiries prove that the system operates successfully, reliably and trouble-free.



#### 1 mixing condenser

- 2 interconnected steam jet ejector (stage 1)
  - 8 process flow
- 3 interconnected mixing condenser
- 4 last ejector (stage 2)
- 5 seal tank

#### 9 overflow (seal tank) 10 to cooling tower

6 motive steam

7 cooling water

#### Without booster

- Design parameter: 100 kg/h water vapour + 10 kg/h air @ 70 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

	· · · · · · · · · · · · · · · · · · ·	
Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37,5 °C	Electrical energy (kW)
78	14.5	

#### With booster

- Design parameter: 100 kg/h water vapour
- + 10 kg/h air @ 40 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37,5 °C	Electrical energy (kW)
135	21.5	

### With booster

- Design parameter: 100 kg/h water vapour + 10 kg/h air @ 40 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

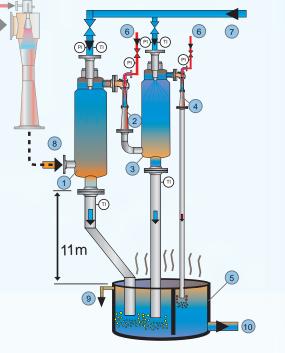
Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37 °C	Electrical energy (kW)
168	33.5	

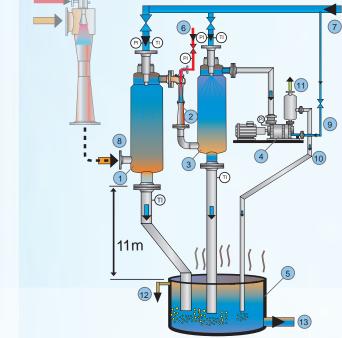
#### Without booster

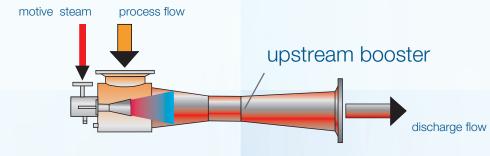
- Design parameter: 100 kg/h water vapour + 10 kg/h air @ 90 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37 °C	Electrical energy (kW)
72	20	

- 1 surface condenser
- 2 interconnected steam jet ejector
- (stage 1) 3 interconnected surface condenser
- 4 last steam jet ejector (stage 2)
- 5 seal tank
- 6 motive steam
- 7 cooling water
- 9 overflow (seal tank)
- 10 to cooling tower

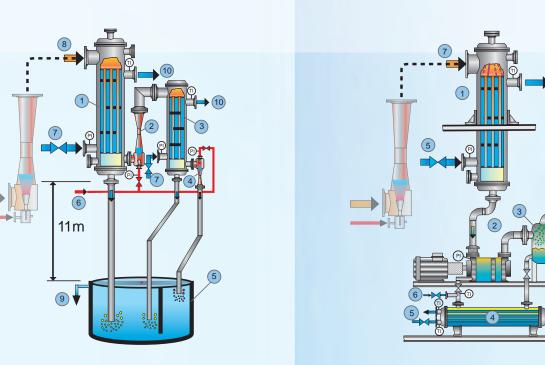






All systems are designed to operate with pre-condensers, but an additional booster can be installed upstream

of the condenser. By means of this installation a vacuum level below 40 mbar is easy to reach.



2 interconnected steam jet ejector (stage 1)

3 interconnected mixing condenser 4 liquid ring vacuum pump (Irvp - stage 2)

5 seal tank

6 motive steam

9 service water (Irvp) 10 overflow (Irvp) 11 gas outlet (Irvp) 12 overflow (seal tank)

13 to cooling tower

8 process flow

#### Without booster

- Design parameter: 100 kg/h water vapour + 10 kg/h air @ 70 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37,5 °C	Electrical energy (kW)
17	12.5	3.5

#### With booster

- Design parameter: 100 kg/h water vapour + 10 kg/h air @ 40 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37,5 °C	Electrical energy (kW)
74	20.5	3.5

#### With booster

- Design parameter: 100 kg/h water vapour + 10 kg/h air @ 40 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37,5 °C	Electrical energy (kW)
98	28.5	7.7

#### Without booster

- Design parameter: 100 kg/h water vapour + 10 kg/h air @ 90 mbar and 80 °C
- motive steam pressure 9 bar (abs)
- cooling water inlet temperature 32 °C

Motive steam (kg/h)	Cooling water (m³/h) 32 °C => 37,5 °C	Electrical energy (kW)
	13	7.7

1 surface condenser

2 liquid ring vacuum pump (lrvp)

3 separator (Irvp)

4 service water re-cooler (Irvp)

9 gas outlet separator (Irvp) 5 cooling water

6 fresh water (Irvp)

7 process flow

8 overflow (Irvp)

10 to cooling tower